

## Heat exchangers, type HE

## Introduction



Heat exchanger type HE is used primarily for heat transfer between the liquid and suction lines of the refrigeration plant.

The purpose is to utilize the cooling effect which without a heat exchanger is otherwise lost to the ambient air via uninsulated suction lines. In the heat exchanger, this effect is used to subcool the refrigerant liquid.

## Features

- High refrigeration capacity in evaporator
- Helps ensure vapour-free liquid ahead of expansion valve.
- Maximum utilisation of evaporator on setting the thermostatic expansion valve for minimum superheat.
- Helps prevent sweating and iced-up suction lines.

## Technical data

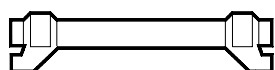
*Refrigerants*  
All fluorinated refrigerants.

*Operating temperature*  
-60 → +120°C

*Max. working pressure*  
HE 0.5, 1.0, 1.5, 4.0: PS = 28 bar  
HE 8.0: PS = 21.5 bar

*Max. test pressure*  
HE 0.5, 1.0, 1.5, 4.0: p' = 40 bar  
HE 8.0: p' = 28 bar

## Ordering



Type	Solder connection ODF				Code no.
	Liquid line		Suction line		
	in.	mm	in.	mm	
HE 0.5		6		12	015D0001
	1/4		1/2		015D0002
HE 1.0		10		16	015D0003
	3/8		5/8		015D0004
HE 1.5		12		18	015D0005
	1/2		3/4		015D0006
HE 4.0		12		28	015D0007
	1/2		1 1/8		015D0008
HE 8.0		16		42	015D0009
	5/8		1 5/8		015D0010

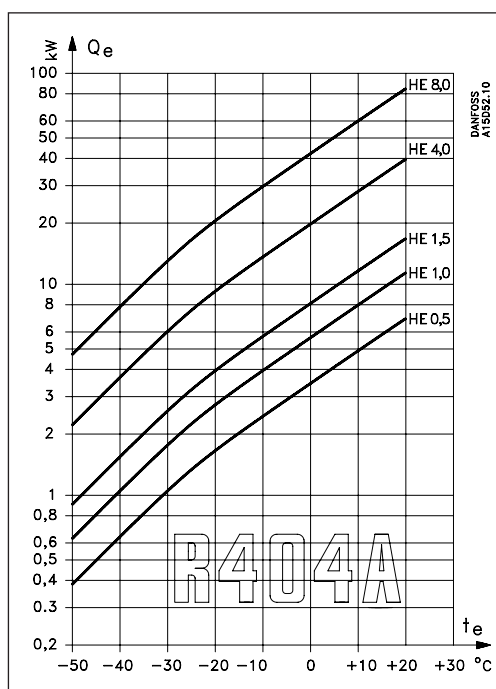
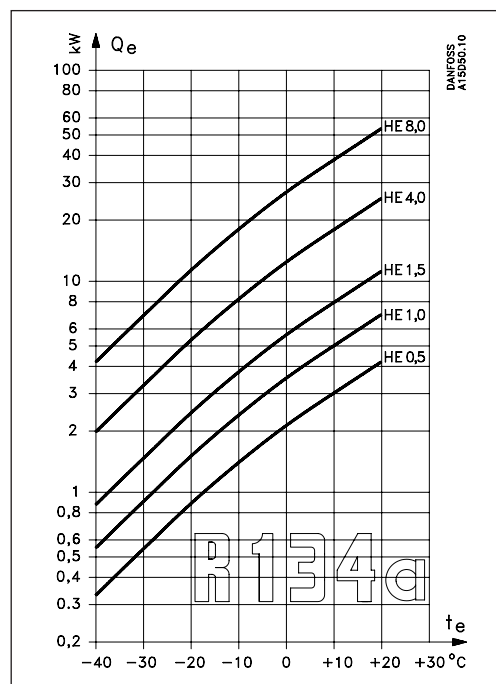
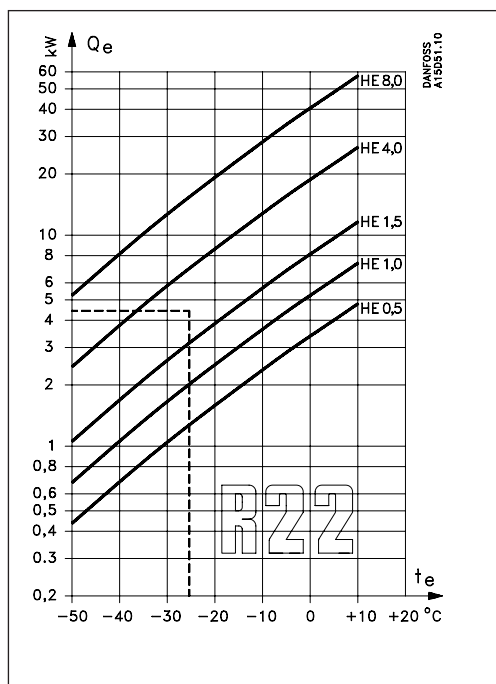
Generally, the size of an HE exchanger can be determined from the connections corresponding to the pipe dimensions of the refrigeration plant.

The design is such that normal suction gas velocities are achieved, with a subsequent small pressure drop. Thus the heat exchanger capacity will match plant capacity.

At the same time, oil return to the compressor is ensured.

If the main object is to avoid sweating and frosting-up of the suction line, the HE can be chosen one size larger than the size determined by the capacity. An HE used as an auxiliary condenser must always be selected according to the connection dimensions.

Capacity



The curve for R22 shows that an HE 4.0 is suitable. The curve for HE 4.0 lies immediately above the intersection of the lines through  $Q_e = 4.5 \text{ kW}$  and  $t_e = -25^\circ\text{C}$ .

The heat flow  $Q$  during heat exchange is calculated from the formula:  $Q = k \times A \times \Delta t_m$   
 $Q$  heat flow in W  
 $k$  heat transfer coefficient in  $\text{W}/\text{m}^2 \text{ } ^\circ\text{C}$   
 $A$  transfer area of the heat exchanger in  $\text{m}^2$   
 $\Delta t_m$  the average temperature difference in  $^\circ\text{C}$ , calculated from the formula:

$$\Delta t_m = \frac{\Delta t_{\max} - t_{\min}}{\ln \frac{\Delta t_{\max}}{\Delta t_{\min}}}$$

$k \times A$  values

Determined by experiment (see table).

Type	K x A
	1) Dry suction gas / refrigerant liquid (normal use in refrigeration plant with fluorinated refrigerants) W / °C
HE 0.5	2.3
HE 1.0	3.1
HE 1.5	4.9
HE 4.0	11.0
HE 8.0	23.0

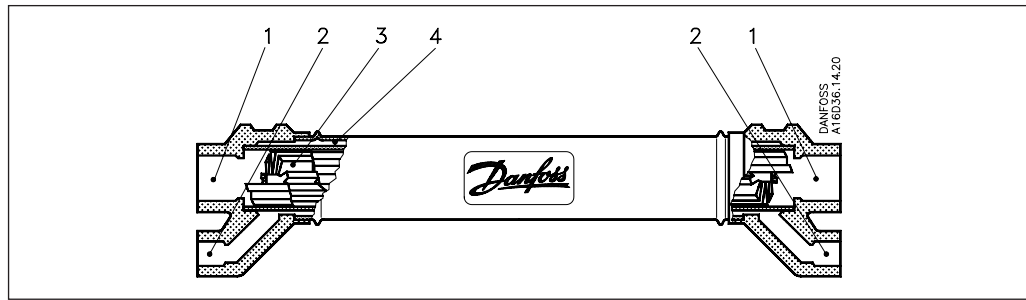
Precise heat exchanger sizing can be obtained from the curves which show plant capacity  $Q_e$  for R22, R134a and R404A depending on evaporating temperature  $t_e$ .

*Example*  
 Plant capacity  $Q_e$  = 4.5 kW  
 Refrigerant = R22  
 Evaporating temperature  $t_e$  =  $-25^\circ\text{C}$

1) These figures apply to dry gas only. Even if a thermostatic expansion valve is used, the suction gas will carry very small liquid drops into the suction line. The fins of the HE catch these drops which then evaporate. This may result in a smaller superheat than the theoretically calculated value.

**Design Function**

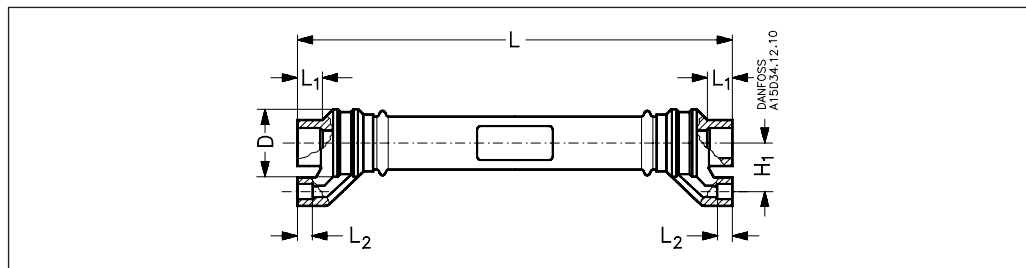
- 1. Suction line connection
- 2. Liquid line connection
- 3. Inner chamber
- 4. Outer chamber



Offset fin sections are built into the inner chamber (3) and result in turbulent gas flow with minimum flow resistance. Gas flow is straight through, without changes of direction and without oil pockets.

Refrigerant liquid flows counter to the gas flow, through the small outer chamber (4). The flow is guided by a built-in wire coil so that maximum heat transfer is achieved. The hot liquid flowing through the outer chamber normally protects the outer tube from "sweating".

**Dimensions and weights**



Type	H <sub>1</sub> mm	L mm	L <sub>1</sub> mm	L <sub>2</sub> mm	∅ D mm	Weight kg
HE 0.5	20	178	10	7	27.5	0.3
HE 1.0	25	268	12	9	30.2	0.5
HE 1.5	30	323	14	10	36.2	1.0
HE 4.0	38	373	20	10	48.3	1.5
HE 8.0	48	407	29	10	60.3	2.3

Type	Volume	
	Outer chamber cm <sup>3</sup>	Inner chamber cm <sup>3</sup>
HE 0.5	8.5	23.0
HE 1.0	25.0	45.0
HE 1.5	40.0	100.0
HE 4.0	80.0	260.0
HE 8.0	175.0	475.0

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